

Environmental Protection Agency

Pt. 63, Subpt. OOO, Table 4

TABLE 3 TO SUBPART OOO OF PART 63—BATCH PROCESS VENT MONITORING REQUIREMENTS

Control device	Parameters to be monitored	Frequency/recordkeeping requirements
Scrubber <sup>a</sup> .....	pH of scrubber effluent, and .....	Continuous records as specified in § 63.1416(d). <sup>b</sup>
	Scrubber liquid and gas flow rates .....	Continuous records as specified in § 63.1416(d). <sup>b</sup>
Absorber <sup>a</sup> .....	Exit temperature of the absorbing liquid, and, .....	Continuous records as specified in § 63.1416(d). <sup>b</sup>
	Exit specific gravity for the absorbing liquid. ....	Continuous records as specified in § 63.1416(d). <sup>b</sup>
Condenser <sup>a</sup> .....	Exit (product side) temperature .....	Continuous records as specified in § 63.1416(d). <sup>a</sup>
Carbon adsorber <sup>a</sup> .....	Total regeneration steam flow or nitrogen flow, or pressure (gauge or absolute) during carbon bed regeneration cycle(s), and, .....	Record the total regeneration steam flow or nitrogen flow, or pressure for each carbon bed regeneration cycle.
	Temperature of the carbon bed after regeneration and within 15 minutes of completing any cooling cycle(s). ....	Record the temperature of the carbon bed after each regeneration and within 15 minutes of completing any cooling cycle(s).
Thermal incinerator .....	Firebox temperature <sup>c</sup> .....	Continuous records as specified in § 63.1416(d). <sup>b</sup>
Catalytic incinerator .....	Temperature upstream and downstream of the catalyst bed. ....	Continuous records as specified in § 63.1416(d). <sup>b</sup>
Boiler or process heater with a design heat input capacity less than 44 megawatts and where the batch process vents or aggregate batch vent streams are not introduced with or used as the primary fuel. ....	Firebox temperature <sup>c</sup> .....	Continuous records as specified in § 63.1416(d). <sup>b</sup>
Flare .....	Presence of a flame at the pilot light .....	Hourly records of whether the monitor was continuously operating during batch emission episodes, or portions thereof, selected for control and whether a flame was continuously present at the pilot light during said periods.
All control devices .....	Diversion to the atmosphere from the control device or, .....	Hourly records of whether the flow indicator was operating during batch emission episodes, or portions thereof, selected for control and whether a diversion was detected at any time during said periods as specified in § 63.1416(d).
	Monthly inspections of sealed valves .....	Records that monthly inspections were performed as specified in § 63.1416(d).
Scrubber, absorber, condenser, and carbon adsorber (as an alternative to the requirements previously presented in this table). ....	Concentration level or reading indicated by an organic monitoring device at the outlet of the control device. ....	Continuous records as specified in § 63.1416(d). <sup>b</sup>

<sup>a</sup> Alternatively, these devices may comply with the organic monitoring device provisions listed at the end of this table.

<sup>b</sup> “Continuous records” is defined in § 63.111.

<sup>c</sup> Monitor may be installed in the firebox or in the ductwork immediately downstream of the firebox before any substantial heat exchange is encountered.

TABLE 4 TO SUBPART OOO OF PART 63—OPERATING PARAMETER LEVELS

Device	Parameters to be monitored	Established operating parameter(s)
Scrubber .....	pH of scrubber effluent; and scrubber liquid and gas flow rates. ....	Minimum pH; and minimum liquid/gas ratio
Absorber .....	Exit temperature of the absorbing liquid; and exit specific gravity of the absorbing liquid. ....	Maximum temperature; and maximum specific gravity
Condenser .....	Exit temperature .....	Maximum temperature

Device	Parameters to be monitored	Established operating parameter(s)
Carbon absorber .....	Total regeneration steam or nitrogen flow, or pressure (gauge or absolute) <sup>a</sup> during carbon bed regeneration cycle; and temperature of the carbon bed after regeneration (and within 15 minutes of completing any cooling cycle(s)).	Maximum flow or pressure; and maximum temperature
Thermal incinerator .....	Firebox temperature .....	Minimum temperature
Catalytic incinerator .....	Temperature upstream and downstream of the catalyst bed.	Minimum upstream temperature; and minimum temperature difference across the catalyst bed
Boiler or process heater .....	Firebox temperature .....	Minimum temperature
Other devices (or as an alternate to the requirements previously presented in this table) <sup>b</sup> .	Organic HAP concentration level or reading at outlet of device.	Maximum organic HAP concentration or reading

<sup>a</sup>25 to 50 mm (absolute) is a common pressure level obtained by pressure swing absorbers.

<sup>b</sup>Concentration is measured instead of an operating parameter.

TABLE 5 TO SUBPART OOO OF PART 63—REPORTS REQUIRED BY THIS SUBPART

Reference	Description of report	Due date
§ 63.1400(j) and Subpart A of this part .....	Refer to Table 1 and Subpart A of this part.	Refer to Subpart A of this part.
63.1417(d) .....	Precompliance Report .....	Existing affected sources—12 months prior to the compliance date. New affected sources—with application for approval of construction or reconstruction.
63.1417(e) .....	Notification of Compliance Status .....	Within 150 days after the compliance date.
63.1417(f) .....	Periodic Reports .....	Semiannually, no later than 60 days after the end of each 6-month period. See § 63.1417(f)(1) for the due date for the first report.
63.1417(f)(12) .....	Quarterly reports upon request of the administrator.	No later than 60 days after the end of each quarter.
63.1417(g) .....	Start-up, shutdown, and malfunction reports.	Semiannually (same schedule as Periodic reports).
63.1417(h)(1) .....	Notification of storage vessel inspection	As specified in 40 CFR part 63, subpart WW.
63.1417(h)(2) .....	Site-specific test plan .....	90 days prior to planned date of test.
63.1417(h)(3) .....	Notification of planned performance test	30 days prior to planned date of test.
63.1417(h)(4) .....	Notification of change in primary product	As specified in § 63.1400 (g)(7) or (g)(8).
63.1417(h)(5) .....	Notification of added emission points .....	180 days prior to the appropriate compliance date.
63.1417(h)(6) .....	Notification that a small control device has been redesignated as a large control device.	Within 60 days of the redesignation of control device size.
63.1417(h)(7) .....	Notification of process change .....	Within 60 days after performance test or applicability assessment, whichever is sooner.

<sup>a</sup>Note that the APPU remains subject to this subpart until the notification under § 63.1400(g)(7) is made.

TABLE 6 TO SUBPART OOO OF PART 63—COEFFICIENTS FOR TOTAL RESOURCE EFFECTIVENESS<sup>A</sup>

Control device basis	Values of coefficients		
	A	B	C
Flare .....	$5.276 \times 10^{-1}$	$9.98 \times 10^{-2}$	$2.096 \times 10^{-3}$
Thermal Incinerator 0 Percent Recovery .....	$4.068 \times 10^{-1}$	$1.71 \times 10^{-2}$	$8.664 \times 10^{-3}$
Thermal Incinerator 70 Percent Recovery .....	$6.868 \times 10^{-1}$	$3.21 \times 10^{-3}$	$3.546 \times 10^{-3}$

<sup>A</sup>Use according to procedures outlined in this section.  
 MJ/scm=MegaJoules per standard cubic meter.  
 scm/min=Standard cubic meters per minute.